

<sup>1</sup>M. Irfan , <sup>1</sup>S. Sadia , <sup>1</sup>J. Bakhtawar ,  
<sup>2</sup>H.A. Shakir , <sup>2</sup>M. Khan , <sup>3</sup>S. Ali 

<sup>1</sup>Department of Biotechnology, University of Sargodha, Sargodha, Pakistan,  
<sup>2</sup>Department of Zoology, University of the Punjab new campus, Lahore, Pakistan,  
<sup>3</sup>Department of Zoology, Government College University, Lahore, Pakistan  
\*e-mail: irfan.ashraf@uos.edu.pk

### Utilization of peanut shells as substrate for cellulase production in submerged fermentation through Box-Behnken Design

**Abstract:** Increasing environmental pollution and global warming encourage bioengineers and biotechnologists to find renewable and environmental friendly sources of energy. Conversion of biomass especially agro-industrial biomass consisting of lignocellulosic material into different products and energy is the modern and promising scheme for this purpose due to their abundance in nature, lower cost and easy handling. These properties made them potential producers of biofuels in near future. In current research, *Bacillus paralichniformis* potential for cellulase production was analyzed using submerged fermentation, for which peanut shell waste was used as a substrate. Nutritional factors were optimized for best enzyme production using Box-Behnken Design (BBD) of response surface methodology (RSM). Results illustrated the maximum enzyme production of 12.838 IU for CMCase and 40.956 IU for FPase after 24 h of fermentation period. These results were obtained at 3 g/mL substrate concentration, 0.45 g/mL yeast extract and 0.01 g/mL MgSO<sub>4</sub> for CMCase and 3g/mL substrate, 0.45 g/mL yeast extract and 0.3 g/mL MgSO<sub>4</sub> for FPase. These results proposed the possibility of utilization of this strain for production of cellulase to endorse its use in industry.

**Key words:** *Bacillus* sp., cellulase, peanut shells, RSM, CCD, submerged fermentation.

#### Introduction

Increasing environmental pollution and global warming encourage bioengineers and biotechnologists to find renewable and environmental friendly sources of energy [1]. Conversion of biomass especially agro-industrial biomass consisting of lignocellulosic material into different products and energy is the modern and promising scheme for this purpose due to their abundance in nature, lower cost and easy handling. These properties made them potential producers of biofuels in near future [2]; if the product recovery and purification steps use limited and optimized water, solvents and energy [3; 4]. On the other hand conversion of lignin gasification (LG) biomass into simple units remains the major problem due to complex chemical nature of LG material. However, enzymatic hydrolysis, physical or biological degradation methods made it easy and economical for industrial uses [5]. These processes effect saccharification of cellulose enzymatically [6]. Cellulose is the most abundant

and naturally renewable source of energy which can compete with many of the existing but expensive and nonrenewable resources of energy. It is a plant biopolymer with complex structure having a hydrolytic enzyme system for the cleavage of bonds and its conversion into simple sugar like D-glucose units [7].

Cellulases are the enzymes that catalyze cellulose into fermentable sugars which is now considered the feasible process to reduce the risk of environmental pollution, easy and useful dumping and degradation of plant and cellulosic waste. In industry these have great importance in paper and pulp, textile, detergents, food and feed additives, bio-ethanol production and processing of chemicals. The prerequisite for easy and economical use of cellulases is to search for best microbial strains which produce high enzyme titer and to optimize media that could be affordable for industry. There are many microorganisms studied and searched for the production of cellulases but lesser number of them are able to produce it in economically feasible

and industrially significant quantities of enzyme [8]. Microorganisms are genetically the most diverse group due to high metabolic flexibility and multiple enzyme based reactions which in turn catalyze complex structures like cellulose in D-glucose with the help of enzymes called cellulase. Microorganisms have high impact on biotechnological applications due to these significant features [7]. Bacteria are emerging as hotspots of versatility and variety genetically and functionally. They can degrade lignocellulosic materials involving complex system of lignocellulolytic enzymes [9].

The complex cellulase enzyme system consists of three enzymes which are endoglucanases, exoglucanases and cellobioases [10]. Endoglucanases are  $\beta$ -1,4-D glucan-4-glucano-hydrolase and carboxymethyl cellulase, while exoglucanases are  $\beta$ -1,4-D glucan-4-gluco-hydrolase and cellobiohydrolase and cellobioases termed as CBH and cellobioases are  $\beta$ -D glucoside glucohydrolase and  $\beta$ -1,4-D-glucosidase, all free enzymes present in 57 of glycosyl hydrolase families [11; 12]. Cellulolytic enzymes would be of great industrial use with the promising environmental and economical sustainability if their media could be improved with the proper optimized conditions for achieving best enzyme titer that eventually lessens its cost [13].

The optimization of cellulase production and selection of ideal substrate are major and important steps having significant enzyme titer at the end. Limited information was available for *Bacillus* species enzymology and its cellulolytic activities. Bacterial cellulases usually reported to be extracellular and production can be optimized by adjusting nutritional parameters and physical properties like temperature and pH, etc. The major factor has always been carbon source but nitrogen phosphorus and metal ions sources are also of great importance [14].

Determination of cellulolytic potential of microorganism is carried out via fermentation process. There are two types used commonly one is solid state fermentation and second is submerged fermentation. Solid state fermentation is carried out in the absence of free liquids as microorganisms grow on firm surfaces holding up as substrates [15]. This type has been used mostly for filamentous fungi where solid substrate acts as natural surface for filamentous growth of fungi [16].

Submerged fermentation usually denoted as SMF is a type of fermentation which requires large amount of liquid substrates as compared to solid state fermentation. These may be water, molasses or

broths. The products which mainly are secondary metabolites or enzymes are secreted in and collected form liquid media. Continuous replenishment of substrates or nutrient may be required according to the use of substrates in fermentation process. Microbes which need high moisture content for their growth such as bacteria usually best for this type of fermentation. The advantage of this technique is easy purification and product recovery [17; 18]. Submerged fermentation is preferred for bacterial cultures due to ease of purification, sterilization and process control. The culture conditions and media optimization are the major steps to be considered [19]. During early 1970's, cellulase production was started commercially via submerged fermentation. Mega scale use of cellulase as animal feed additive and for stonewashing denim was practiced in industry during 1980's [20].

Formulation of media is specific for the organism and its optimization is necessary for best production of required substance hence any general media composition cannot be used for optimum growth and cellulase production [21]. Response surface methodology (RSM) is the statistical analysis modeling used to optimize and evaluate many biotechnological processes and enzymatic hydrolysis [22]. RSM is affected by many parameters and variable factors affecting the results and then these are optimized for the best conditions using different designs of RSM with the interpolation of first or second polynomial equations in sequential testing procedure [23; 24]. This technique, RSM integrates mathematical and statistical approaches and analyzes defined independent parameters on response without having any previous information about the relation between response function and variable parameters [25-27]. RSM is being used now statistically, as an appropriate methodology for experiment designing, statistical model building, evaluation of factors affecting the optimum conditions for required response and in turn, decreasing the number of experiments for the required response [28]. In biotechnological processes, RSM evaluate the optimum conditions for the growth of microorganism and product formation [29; 30]. Here, RSM was used to determine optimal conditions for novel bacterial strain *Bacillus parlichniformis* and the factors that affect the response of cellulase production. Peanut shell waste has been taken as carbon source and cellulolytic potential of *Bacillus parlichniformis* was investigated in submerged fermentation with optimal medium conditions.

## Materials and methods

**Object.** Samples of *Bacillus paralichniformis* isolated from soil were provided by the Laboratory of Microbial Biotechnology, Department of Biotechnology, University of Sargodha. The strain was maintained on nutrient agar slants and used for cellulase production in subsequent study.

**Enzyme production.** Submerged fermentation was performed for the production of enzyme having medium ingredients of peanut shell waste, yeast extract and MgSO<sub>4</sub>. Concentration of these ingredients was optimized as per experimental design. The medium components were sterilized and inoculated with 1ml of 24 h old vegetative cell culture and placed in a shaking incubator for 24 h with a shaking speed of 120 rpm at 35°C. Culture broth was consequently centrifuged at 10,000 x g and 4°C for 10 min. Centrifuged pure extract without cellular material was used as source of crude enzyme extract for further processing.

**Cellulase assay.** Carboxymethyl cellulase (CMCase) and filter paper activity (FPase) was estimated as described in our earlier reports [31].

**Saccharification of peanut shell.** In 500 mL conical flask, 100 mL of crude cellulase enzymes with 4% substrate was incubated at 50 °C for various time intervals. After termination of enzymatic hydrolysis, centrifugation of material was performed at 10,000 rpm for 10 min. Saccharification (%) was calculated using the following formulae [32].

$$\text{Saccharification (\%)} = \frac{\text{Reducing sugars released (mg/ml)}}{\text{Substrate used (mg/ml)}} \times 100$$

**Experimental design.** Box–Behnken design (BBD) was used for optimization of medium components in this study. The independent and noteworthy variables used were peanut shell (substrate) concentration (X<sub>1</sub>), yeast concentration, (X<sub>2</sub>) and MgSO<sub>4</sub> (X<sub>3</sub>) and their levels are mentioned in Table 1. The relation between actual and coded values was described by the following equation;

$$x_i = \frac{X_i - X_0}{\Delta X_i}$$

where x<sub>i</sub> and X<sub>i</sub> are the coded and actual values of the independent variable, X<sub>0</sub> is the actual value of the independent variable at the center point and ΔX<sub>i</sub> is the change of X<sub>i</sub>. The response is calculated from

the following equation using STATISTICA software (99th ed.).

$$Y = \beta_0 + \beta_1 X_1 + \beta_2 X_2 + \beta_3 X_3 + \beta_{11} X_1^2 + \beta_{22} X_2^2 + \beta_{33} X_3^2 + \beta_{12} X_1 X_2 + \beta_{13} X_1 X_3 + \beta_{23} X_2 X_3$$

Y is the response, X<sub>1</sub>, X<sub>2</sub> and X<sub>3</sub> are the independent variables, β<sub>0</sub> is the intercept, β<sub>1</sub>, β<sub>2</sub> and β<sub>3</sub> are linear coefficient, β<sub>1</sub><sup>2</sup>, β<sub>2</sub><sup>2</sup> and β<sub>3</sub><sup>2</sup> are square coefficients, β<sub>12</sub>, β<sub>13</sub> and β<sub>23</sub> are interaction coefficients.

## Results and discussion

Cellulases were produced by *Bacillus paralichniformis* in SMF. Media optimization for best enzyme titer was carried out using three independent variables such as substrate (peanut shell waste) concentration (X<sub>1</sub>), Yeast extract (X<sub>2</sub>) and MgSO<sub>4</sub> (X<sub>3</sub>) and their levels are mentioned in Table 1. The response was calculated by second degree polynomial regression equation (Eq. 3; 4) using Minitab software version 9.

With the optimized conditions of media, the best enzyme production obtained for CMCase was 12.838 IU with optimized conditions of substrate concentration of 3 (%), yeast extract 0.45 (%) and MgSO<sub>4</sub> 0.01(%) after 24 h of incubation. This value was in close proximity with the predicted value of 12.38850 IU as shown in table 2. Highest FPase production (40.956 IU) was observed with substrate concentration of 3 (%), 0.45% of yeast extract and MgSO<sub>4</sub> concentration of 0.3 (%) having predicted value of 31.5108 IU.

**Table 1** – Coded and actual levels of the factors for three factors Box-Behnken design

Independent variables	Symbols	Coded and actual values		
		-1	0	+1
Peanut shell waste	X <sub>1</sub>	0.5	1.75	3
Yeast extract	X <sub>2</sub>	0.1	0.45	0.8
MgSO <sub>4</sub>	X <sub>3</sub>	0.01	0.155	0.3

$$\begin{aligned} \text{CMCase (IU)} = & -3.55 + 7.13 X_1 + 18.15 X_2 \\ & + 12.96 X_3 - 0.574 X_1 * X_1 - 19.62 X_2 * X_2 - \\ & 64.2 X_3 * X_3 - 3.366 X_1 * X_2 - 4.59 X_1 * X_3 \\ & + 20.59 X_2 * X_3 \text{Equation (3)} \end{aligned}$$

$$\begin{aligned} \text{FPase (IU)} = & 10.7 + 4.5 X_1 + 30.4 X_2 - 40 X_3 \\ & + 1.36 X_1 * X_1 - 40.4 X_2 * X_2 - 141 X_3 * X_3 - 9.8 X_1 * X_2 \\ & + 17.1 X_1 * X_3 + 88 X_2 * X_3 \text{Equation (4)} \end{aligned}$$

**Table 2** – Cellulase production by *B. paralicheniformis* using Box-Behnenken design from peanut shells

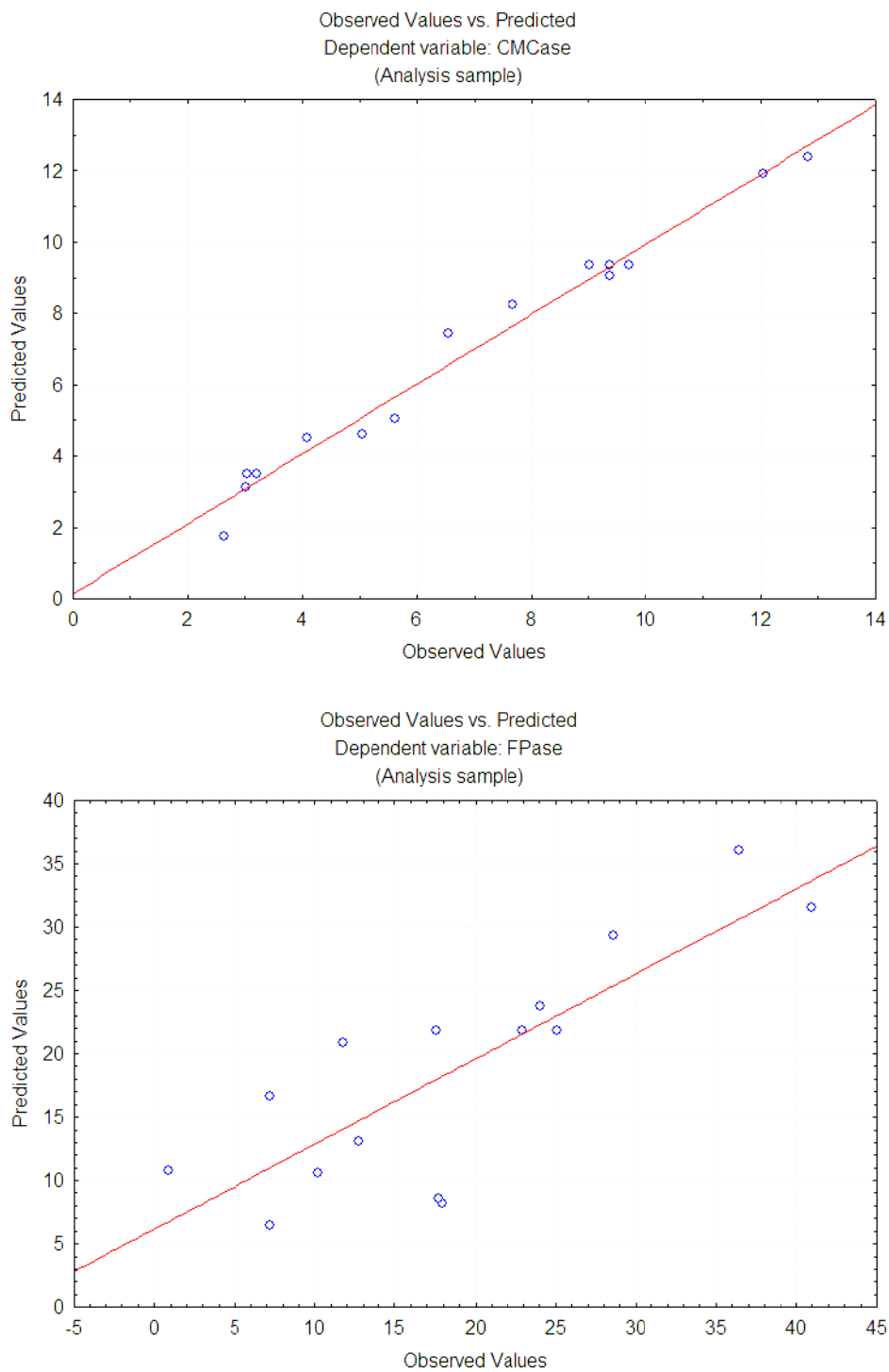
Run #	X <sub>1</sub>	X <sub>2</sub>	X <sub>3</sub>	CMCase activity (IU)			FPase activity (IU)		
				Observed	Predicted	Residual	Observed	Predicted	Residual
1	0.5	0.45	0.01	3.204	3.49975	-0.29575	7.238	16.68313	-9.4451
2	1.75	0.8	0.01	5.04	4.61963	0.420375	17.979	8.13738	9.84162
3	0.5	0.45	0.3	3.055	3.50450	-0.44950	7.238	6.48912	0.74888
4	3	0.8	0.155	6.557	7.42688	-0.86987	11.746	20.83875	-9.0927
5	0.5	0.8	0.155	3.024	3.14863	-0.12462	10.2	10.59650	-0.3965
6	1.75	0.1	0.3	4.085	4.50538	-0.42037	0.901	10.74263	-9.8416
7	3	0.45	0.3	9.358	9.06225	0.295750	40.956	31.51088	9.44513
8	3	0.1	0.155	12.043	11.91838	0.124625	36.45	36.05350	0.39650
9	1.75	0.45	0.155	9.358	9.36167	-0.00366	17.541	21.84300	-4.3020
10	1.75	0.45	0.155	9.019	9.36167	-0.34266	25.063	21.84300	3.22000
11	3	0.45	0.01	12.838	12.38850	0.449500	28.592	29.34088	-0.7488
12	1.75	0.1	0.01	7.682	8.25613	-0.57412	24.084	23.73163	0.35237
13	1.75	0.8	0.3	5.623	5.04888	0.574125	12.75	13.10238	-0.3523
14	1.75	0.45	0.155	9.708	9.36167	0.346333	22.925	21.84300	1.08200
15	0.5	0.1	0.155	2.62	1.75013	0.869875	17.709	8.61625	9.09275

All the data was statistically analyzed using analysis of variance for significance of the model (Table 3). The significance of model and response for coefficients is mainly dependent on F-value and P-values. The higher the F-value resulting in lower P-value described the high accuracy and significance of regression model [33]. Therefore, higher computed Fischer's F-value for CMCase was 26.07 and for FPase 1.14 with P-value 0.001 and 0.468 respectively. The model for CMCase was highly significant while FPase was found not significant. The fitness of model was further analyzed by the determination coefficient R<sup>2</sup> for CMCase and FPase. The R<sup>2</sup> value for CMCase and FPase were 97.91% and 67.17%, which revealed that 2.09% and 32.67% variation was not determined by model respectively. Higher value of R square of CMCase showed the accuracy of the model (Figure 1).

*Interaction effect of parameters.* The interaction effect of substrate concentration (X<sub>1</sub>), yeast extract

(X<sub>2</sub>) and MgSO<sub>4</sub>(X<sub>3</sub>) has been described in contour plots. Different pattern of colors in these plots depicted levels of enzyme production with one variable constant or zero level and two parameters with different levels (Figure 2). These plots indicated that each parameter significantly affect enzyme production.

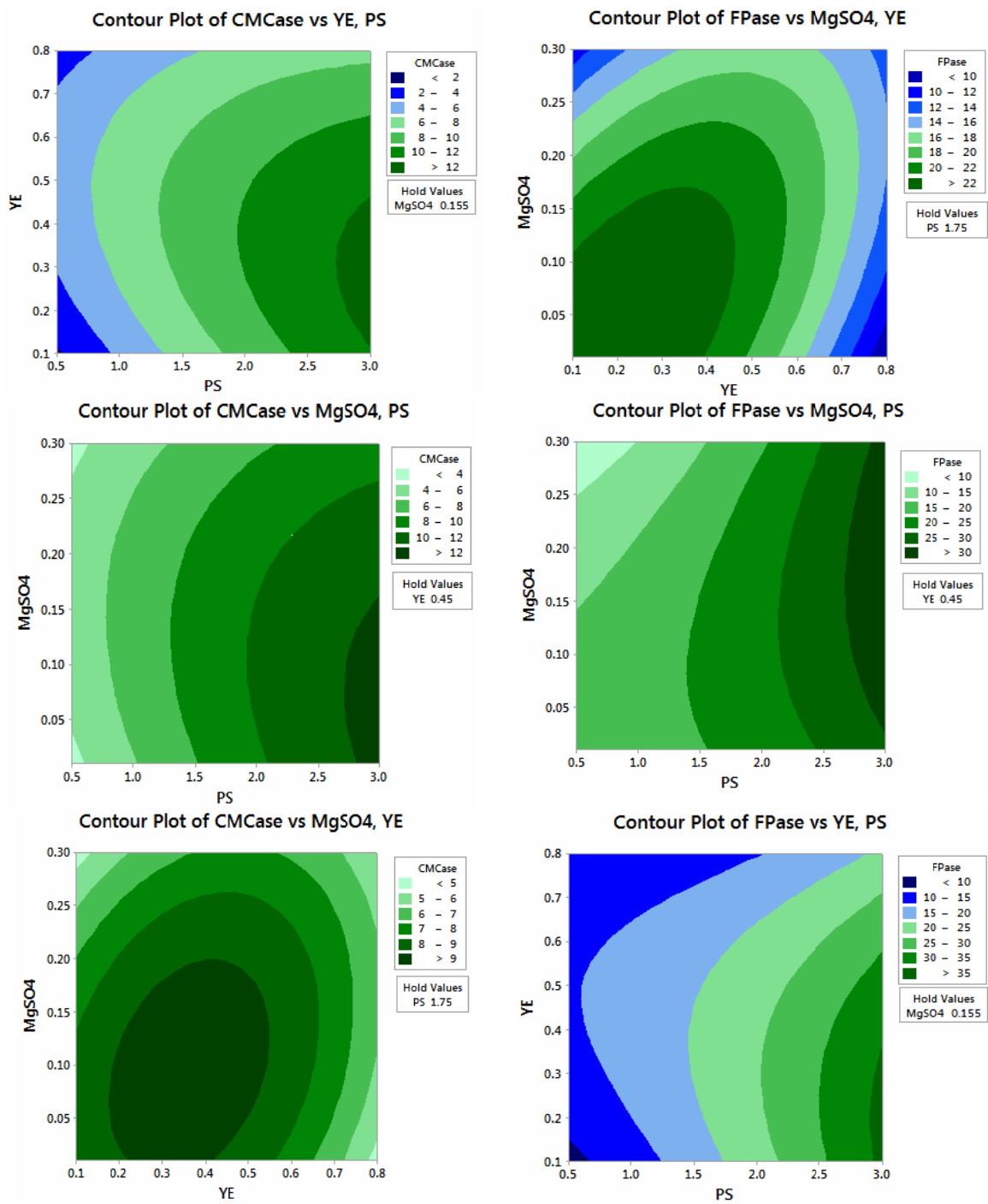
The results were validated further by repeated experiments of optimized values of significant parameters as predicted in desirability diagrams (Figure 3). Results were in the close range with predicted values. This figure depicted that at optimized levels of peanut shell waste 1.75%, yeast extract 0.45% and MgSO<sub>4</sub> 0.155%, the maximum CMCase production was 13.678 IU which was confirmed by repeated experiments. The predicted optimized value for FPase was 1.75% peanut shell waste, 0.45% yeast extract and 0.155% MgSO<sub>4</sub> yielded 41.016 IU enzyme production which were almost similar after experiments.



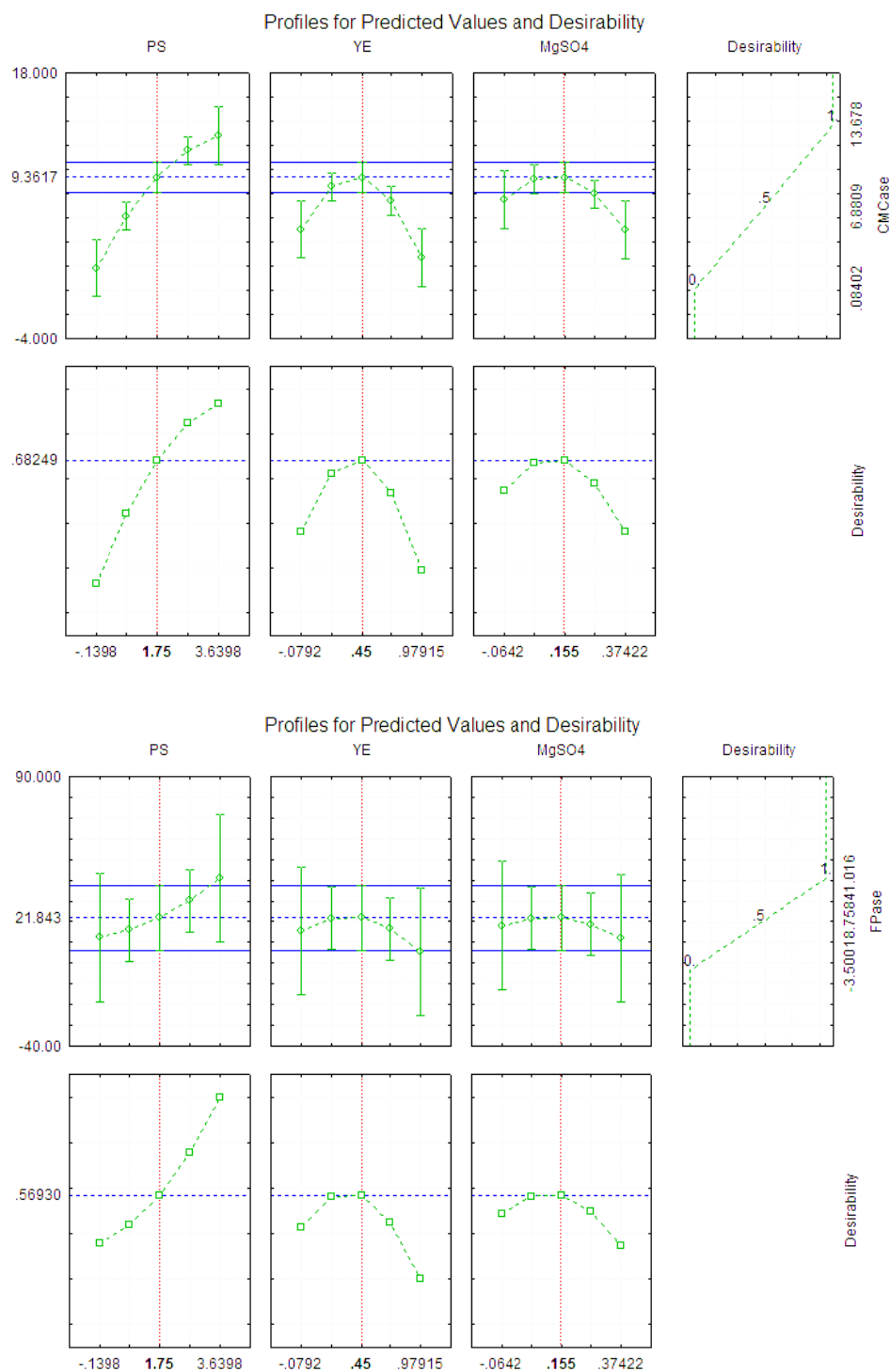
**Figure 1** – Observed vs predicted values of independent variables for maximum enzyme production

**Table 3** – Analysis of variance for cellulase production from *B.paralichniformis* in submerged fermentation

CMCase (IU)	Sources	DF	Adj SS	Adj MS	F value	P value
	Model	9	158.320	17.591	26.07	0.001
	Linear	3	114.650	38.217	56.64	0.000
	X <sub>1</sub>	1	104.351	104.351	154.66	0.000
	X <sub>2</sub>	1	4.783	4.783	7.09	0.045
	X <sub>3</sub>	1	5.516	5.516	8.18	0.035
	Square	3	27.855	9.285	13.76	0.008
	X <sub>1</sub> <sup>2</sup>	1	2.972	2.972	4.41	0.090
	X <sub>2</sub> <sup>2</sup>	1	21.329	21.329	31.61	0.002
	X <sub>3</sub> <sup>2</sup>	1	6.736	6.736	9.98	0.025
	2 Way interaction	3	15.815	5.272	7.81	0.025
	X <sub>1</sub> *X <sub>2</sub>	1	8.673	8.673	12.85	0.016
	X <sub>1</sub> *X <sub>3</sub>	1	2.774	2.774	4.11	0.098
X <sub>2</sub> *X <sub>3</sub>	1	4.368	4.368	6.47	0.052	
Error	5	3.374	0.675	8.81	0.104	
Lack of fit	3	3.136	1.045			
Pure error	2	0.237	0.119			
Total	14	161.693				
FPase (IU)	<b>Sources</b>	<b>DF</b>	<b>Adj SS</b>	<b>Adj MS</b>	<b>F value</b>	<b>P value</b>
	Model	9	1164.71	129.41	1.14	0.468
	Linear	3	829.64	276.55	2.43	0.181
	X <sub>1</sub>	1	709.87	709.87	6.24	0.055
	X <sub>2</sub>	1	87.58	87.58	0.77	0.421
	X <sub>3</sub>	1	32.19	32.19	0.28	0.618
	Square	3	142.35	47.45	0.42	0.749
	X <sub>1</sub> <sup>2</sup>	1	16.76	16.76	0.15	0.717
	X <sub>2</sub> <sup>2</sup>	1	90.37	90.37	0.79	0.414
	X <sub>3</sub> <sup>2</sup>	1	32.51	32.51	0.29	0.616
	2 way interaction	3	192.72	64.24	0.56	0.662
	X <sub>1</sub> *X <sub>2</sub>	1	73.92	73.92	0.65	0.457
	X <sub>1</sub> *X <sub>3</sub>	1	38.22	38.22	0.34	0.587
X <sub>2</sub> *X <sub>3</sub>	1	80.59	80.59	0.71	0.439	
Error	5	569.22	113.84	11.96	0.078	
Lack of fit	3	539.18	179.73			
Pure error	2	30.05	15.02			
Total	14	1733.93				



**Figure 2** – Contour plots for CMCase (IU) and FPase (IU) production from peanut shells by *Bacillus paralicheniformis* submerged fermentation

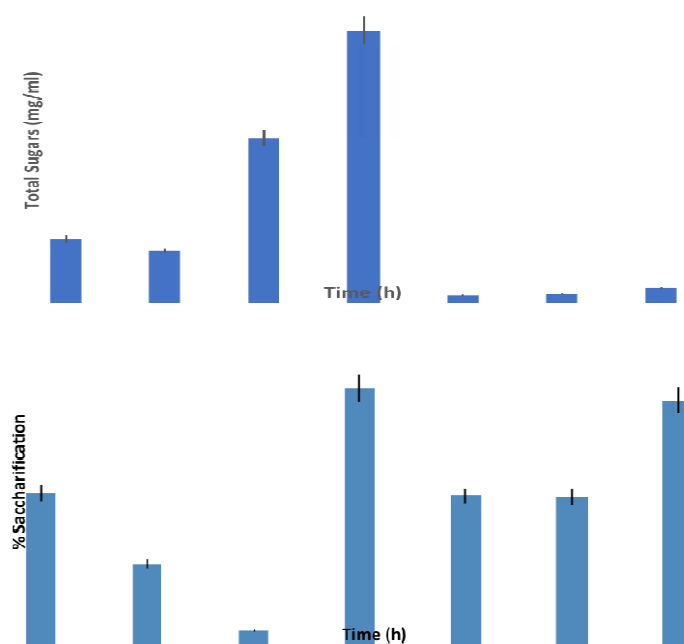


**Figure 3** – Desirability of CMCCase and FPFase production

*Saccharification.* The crude enzyme which was produced from *Bacillus paralichniformis* in submerged fermentation was applied to hydrolyze peanut shell waste. The experiment was carried out for

different time periods and results (Figure 4) depicted the maximum total sugar ( $38.0 \pm 0.23$  mg/mL) production was observed at 8 h. Further increased time of incubation declined sugar production.





**Figure 4** – Sugars released after enzymatic hydrolysis at various time period

As we know cellulase has major industrial role and now the increasing demands of renewable energy sources motivate biotechnologist to search for novel and better microbial strains and easy renewable sources of substrate, like agro-industrial wastes for the production of enzymes, using novel strain. *Bacillus subtilis* K18 had tremendous potential of cellulase production using a variety of substrates like saw dust [34], eucalyptus leaves [35], cotton stalk, peanut shells [36], potato peels [46], *Saccharum spontaneum* [37] and banana peduncle [31] through response surface methodology. Another study reported 0.037 IU/mL/min of CMCase from *Bacillus* sp. C1AC5507 using bagasse through RSM in submerged fermentation [38]. *Bacillus aquimaris* isolated from the gut of *Labeo rohita* has maximum endoglucanase producing potential of 437.3833 IU/mL/min in submerge fermentation [39].

*Bacillus pumilis* strain had potential of using sugarcane bagasse as carbon source for CMCase 13.6 IU/mL/min production in submerge fermentation [40]. *Aeromonas bestiarum* isolated from the gut of *Labeo rohita* gave the endoglucanase titer of 3.766 IU using sugarcane bagasse as substrate [41]. Medium components and type of substrate significantly affects cellulase production in submerge fermentation as described in previous study [42].

The ongoing study has been carried out with this perspective of easily available and renewable plus economical agro waste, i.e. peanut shell waste with a novel strain of *Bacillus paralichniformis*. The cellulase enzyme produced from this bacterium was further used for saccharification of peanut shells, which gave maximum sugar after 8 h of incubation period (Figure 4).

Another study reported maximum sugar production at 6 h for sugar beet pulp [43]. Saccharification of *Saccharum spontaneum* releasing maximum total sugars of 12.71 mg/mL after 20 h of incubation at 50°C [37]. Cellulase produced by the *Bacillus subtilis* K-18 has stimulated the 54.389% saccharification of pine needles [44]. Cellulase mediated saccharification by *Bacillus cereus* produced maximum total sugars of 31.42 mg/mL released after 6 h of incubation at 50 °C [45]. Wheat straw fermented with *Saccharomyces cerevisiae* under optimized condition of 2 % wheat straw, 0.5% enzyme concentration and 6 h of time period has been resulted in 40.15 % of saccharification [33]. Asghar et al. also reported 8 h of incubation time for maximum saccharification of wheat straw [46].

## Conclusion

Results obtained within the current study prove that the novel strain *Bacillus paralichniformis* has

good industrial potential for cellulase production to perform cellulolytic functions, and it can also be used to convert lignocellulosic biomass into ethanol by saccharification.

### Acknowledgment

This study was supported by Office of Research, Innovation and Commercialization, University of Sargodha, wide grant number UOS/ORIC/2016/39.

### References

- Zhang W., Barone R. and Renneckar S. (2016). Enhanced enzymatic saccharification of pretreated biomass using glycerol thermal processing (GTP). *Bioresour Technol.*, vol. 199, pp. 148-154.
- Bhalla A., Bansal N., Kumar S., Bischoff M. and Sani K. (2013). Improved lignocellulose conversion to biofuels with thermophilic bacteria and thermostable enzymes. *Bioresour Technol.*, vol.128, pp. 751-759.
- Barakat A., de Vries H. and Rouau X. (2013). Dry fractionation process as an important step in current and future lignocellulose biorefineries: a review. *Bioresour Technol.*, vol. 134, pp. 362-373.
- Sun F., Zhao X., Hong J., Wang L., Sun H. (2016). Industrially relevant hydrolyzability and fermentability of sugarcane bagasse improved effectively by glycerol organosolv pretreatment. *Biotechnol Biofuels*, vol. 9, pp. 1-13.
- Chen M., Jia Z., Hu H., Zhao B. and Liu H. (2015). A comparison of several organosolv pretreatments for improving the enzymatic hydrolysis of wheat straw: substrate digestibility, fermentability and structural features. *Appl Energy*, vol. 150, pp. 224-232.
- Barakat A., Chuetor S., Monlau F., Solhy A. and Rouau X. (2014). Eco-friendly drychemo-mechanical pretreatments of lignocellulosic biomass: impact on energy and yield of the enzymatic hydrolysis. *Appl Energy*, vol.113, no.1, pp. 97-105.
- Hussain S., Siddique T., Saleem M., Arshad M. and Khalid A. (2009). Impact of Pesticides on Soil Microbial Diversity, Enzymes, and Biochemical Reactions. *Adv Agron.*, vol.102, pp. 160-190.
- Shin C.S., Lee J.P., Lee J.S. and Park S.C. (2000). Enzyme production of *Trichoderma reesei* Rut C-30 on various lignocellulosic substrates. *Appl Biochem Biotechnol.*, pp. 237-245
- López-Mondéjar R., Algora C. and Baldrian P. (2019). Lignocellulolytic systems of soil bacteria: a vast and diverse toolbox for biotechnological conversion processes. *Biotechnol adv.*, vol.37, no. 6, 03.013.
- Joachim H.J., Patrick A.N. (2008). Selected soil enzymes: examples of their potential roles in the ecosystem. *Afr J Biotechnol.*, vol. 7, no. 3, pp.181-191.
- Siddiqui K.S., Saqio A.A.N., Rashid M.H. and Rajoka M.I. (2000). Carboxyl group modification significantly altered the kinetic properties of purified carboxymethyl cellulase from *Aspergillus niger*. *Enzyme Microb Technol.*, vol. 27, pp. 467-474.
- Rashid B., Baba Z.A., Malik M.A., Mir A.H., Akhter F., Asif M., Zargar M.Y., Rashid N., Rashid N. and Maqbool S. (2019). Characterization of cellulolytic bacteria from waste dumping sites of Kashmir Himalaya. *Int J Curr Microbiol App Sci.*, vol. 8, no. 01, pp. 2033-2048.
- Patel A.K., Singhania R.R., Sim S.J. and Pandey A. (2019). Thermostable cellulases: current status and perspectives. *Bioresour Technol.*, vol. 279, pp. 385-392.
- Sreeja S.J., Jeba Malar P.W., Sharmila Joseph F.R., Steffi T., Grasian I. and Palavesam A. (2013). Optimization of cellulase production by *Bacillus altitudinis*. APS MSU and *Bacillus licheniformis* APS2 MSU, gut isolates of fish *Etrophus suratensis*. *IJOART*, vol. 2, pp. 401-406.
- Jecu L, (2000). Solid state fermentation of agricultural wastes for endoglucanase production. *Ind Crops Prod.*, vol. 11, no. 1, pp. 1-5.
- Sajith S., Priji P., Sreedevi S., and Benjamin S. (2016). An overview on fungal cellulases with an industrial perspective. *J Nutr Food Sci.*, vol. 6, no.1, p. 461.
- Sirohi R., Singh A. and Malik S. (2018). Production, characterization and industrial applications of cellulase derived from agro-waste. *Cur J Appl Sci Tech.*, pp. 1-9.
- Subramaniam and Vimala R (2012). Solid state and submerged fermentation for the production of bioactive substances; a comparative study. *Int J Sci Nat.*, vol. 3, no. 3, pp. 480-486.
- Vidyalakshmi R., Paranthaman R. and Indhumathi J. (2009). Amylase production on submerged fermentation by *Bacillus spp.* *World J Chem.*, vol. 4, no.1, pp. 89-91.

20. Tolan J.S. and Foody B. (1999). Cellulase from submerged fermentation. In: Recent progress in bioconversion of lignocellulosics. Springer, Berlin, Heidelberg, pp. 41-67.
21. Tholudur A., Ramirez W.F. and McMillan J.D. (1996). Mathematical modeling and optimization of cellulase protein production using *Trichoderma reesei* RL-P37, *Biotechnol Bioeng.*, vol. 66, no.1, pp. 1-16.
22. Alvira P., Tomás-Pejó E. and Ballesteros M. (2010). Pretreatment technologies for an efficient bioethanol production process based on enzymatic hydrolysis. *Biores Technol.*, vol. 101, pp. 4851-4861.
23. Li C., Knierim B. and Manisseri C. (2007). Comparison of dilute acid and ionic liquid pretreatment of switchgrass: biomass recalcitrance, delignification and enzymatic saccharification. *Biores Technol.*, vol. 101, pp. 4900-4906.
24. Ferreira S., Duarte A.P., Ribeiro M.H., Queiroz J.A. and Domingues F.C. (2009). Response surface optimization of enzymatic hydrolysis of *Cistus ladanifer* and *Cytisus striatus* for bioethanol production. *Biochem Eng J.*, vol. 45, pp. 192-200.
25. Puri S., Beg Q.K. and Gupta R. (2002). Optimization of alkaline protease production from *Bacillus sp.* by response surface methodology. *Curr Microbiol.*, vol. 44, pp. 286-290.
26. Balusu R., Paduru R.R., Kuravi S.K., Seenayya G. and Reddy G. (2005). Optimization of critical medium components using response surface methodology for ethanol production from cellulosic biomass by *Clostridium thermocellum* SS19. *Process Biochem.*, vol. 40, pp. 3025-3030.
27. Wang Q., Ma H., Xu W., Gong L., Zhang W. and Zou D. (2008). Short communication: ethanol production from kitchen garbage using response surface methodology. *Biochem Eng J.*, vol. 39, pp. 604-610.
28. Coninck D.J., Bouquelet S., Dumortier V., Duyme V., Verdier and Denantes I. (2000). Industrial media and fermentation processes for improved growth and protease production by *Tetrahymena thermophila*. *J. Ind. Microbiol. Biotechnol.*, vol. 24, pp. 285-290.
29. Mei X., Liu R., Shen F and Wu H. (2009). Optimization of fermentation conditions for the production of ethanol from stalk juice of sweet sorghum by immobilized yeast using response surface methodology. *Energy Fuels*, vol. 23, pp. 487-491.
30. Shankar T. and Isaiarasu L. (2012). Statistical optimization for cellulase production by *Bacillus pumilus* EWBCM1 using response surface methodology. *Global J Biotech and Biochem.*, vol. 7, no.1, pp. 01-06.
31. Arooj A., Irfan M., Tabsum F., Shakir H.A., Qazi J.I. (2017). Effect of dilute sulphuric acid pretreatment on cellulase production by *Bacillus subtilis* K-18 through response surface methodology. *Proc Pak Ac Sci B; Life and Env Sci.*, vol. 54, no. 1, pp. 11-20.
32. Irfan M., Asghar U., Nadeem M., Nelofer R., Syed Q., Shakir H.A. and Qazi J.I. (2016). Statistical optimization of saccharification of alkali pretreated wheat straw for bioethanol production. *Waste Biomass Valor.*, vol. 7, pp.1389-1396.
33. Long C., Ou Y., Guo P., Liu Y., Cui J., Long M. and Hu Z. (2009). Cellulase production by solid state fermentation using bagasse with *Penicillium decumbens* L-06. *Annals Microbiol.*, vol. 59, pp. 517-523.
34. Anjum A., Irfan M., Tabsum F., Shakir Ha and Qazi J.I. (2017). Optimization of sulphuric acid pre-treatment of *Acacia* saw dust through Box-Bhenken Design for cellulase production by *B.subtilis*. *Adv Life Sci.*, vol. 5, no. 1, pp.19-24.
35. Iqbal S., Irfan M., Tabassum F., Shakir H.A., Qazi J.I. (2017). Application of Box-Behnken Design for optimization of different pretreatment conditions for cellulase production. *J Northeast Agric Univ. (eng.)*, vol. 24, no. 3, pp. 51-59.
36. Arshad F., Irfan M., Shakir H.A., Tabsum F. and Qazi J.I. (2017). Optimization of dilute sulphuric acid pre-treatments of peanut shells through Box-Bhenken Design for cellulase production by *Bacillus subtilis* K-18. *Punjab Univ J Zool.*, vol. 32, no. 1, pp. 81-90.
37. Ghazanfar M., Irfan M., Tabssum F., Shakir H.A. and Qazi J.I. (2018). Effect of different pretreatment conditions on *Saccharum spontaneum* for cellulase production by *B. subtilis* K-18 through Box-Bhenken Design. *Iran J Sci Technol A.*, vol. 42, no. 2, pp. 313-320.
38. Padilha Q.M., Carvalho L.C.T., Dias P.V.S., Grisi C.S.L., Honorato da Silva F.L., Santos S.F.M. and Araujo D.A.M. (2015). Production and characterization of thermophilic carboxymethyl cellulase synthesized by *Bacillus sp.* growing in sugarcane bagasse in submerged fermentation. *Braz J Chem.*, vol. 32, no. 1, pp. 35-42.
39. Khalid S., Irfan M., Shakir H.A., Qazi J.I. (2017). Endoglucanase producing potential of *Bacillus* species isolated from the gut of *Labeo rohita*. *J Mar Sci Tech.*, vol. 25, no. 5, pp. 581-587.
40. Chaudhary N., Qazi J.I. and Irfan M. (2017). Isolation and Identification of Cellulolytic

and Ethanologenic Bacteria from Soil. *Iran J Sci Technol Trans Sci.*, vol. 41, pp. 551-555.

41. Majeed H.S., Irfan M., Shakir H.A. and Qazi J.I. (2016). Filter paper activity producing potential of *Aeromonas* species isolated from the gut of *Labeo rohita*. *Pak J Zool.*, vol. 48, no. 5, pp. 1317-1323.

42. Arshad M., Irfan M., Rehman A., Nadeem M., Huma Z., Shakir H.A., Syed Q. (2017) Optimization for medium and substrate for CMCase production by *Bacillus subtilis* – BS06 in submerged fermentation and its applications in saccharification. *Punjab Univ J Zool.*, vol. 32, no.2, pp. 179-188.

43. Berłowska J., Pielech-Przybylska K., Balcerek M., Dziekońska-Kubczak U., Patelski P., Dziugan P. and Kręgiel D. (2016). Simultaneous saccharification and fermentation of sugar beet pulp

for efficient bioethanol production. *BioMed Res Int.*, 2016.

44. Irfan M., Mushtaq Q., Tabssum F., Shakir H.A. and Qazi J.I. (2017). Carboxymethyl cellulase production optimization from newly isolated thermophilic *Bacillus subtilis* K-18 for saccharification using response surface methodology. *AMB Express*, vol. 7, no. 1, p. 29.

45. Tabssum F., Irfan M., Shakir H.A., Qazi J.I. (2018). RSM based optimization of nutritional conditions for cellulase mediated Saccharification by *Bacillus cereus*. *J Med Biol Eng.*, vol. 12, no. 1, p. 7.

46. Asghar M., Irfan M., Iram Z., Huma R. Nelofer, Nadeem M., Syed Q. (2015). Effect of alkaline pretreatment on delignification of wheat straw. *Nat Prod Res.*, vol.29, no.2, pp. 125-131.